$$j_1|_{x=0} = \sqrt{\frac{D}{\pi t}} (c_{10} - c_{1n})$$

The concentration at the surface is given by Henry's Law:

$$c_{10} = \frac{p}{H} = \frac{0.93 \text{ atm}}{37000 \frac{\text{cm}^3 \text{ atm}}{\text{mol}}} = 2.5 \cdot 10^{-3} \frac{\text{mol}}{\text{cm}^3}$$

Since we have a semiinfinite slab we assume  $c_{1w} = 0$ . To find the flux over the total time t, we integrate:

$$N_{i} = \int_{0}^{t} A f_{i}|_{z=0} dt = A \int_{0}^{t} \sqrt{\frac{D}{\pi t}} (c_{10} - 0) dt = A c_{10} \sqrt{\frac{D}{\pi}} \int_{0}^{t} \frac{dt}{\sqrt{t}} = 2 A c_{10} \sqrt{\frac{D}{\pi}} [\sqrt{t}]_{0}^{t} = 2 A c_{10} \sqrt{\frac{Dt}{\pi}} [\sqrt{t}]_{0}^{t} =$$

Assuming an ideal gas, the flux  $N_I$  is given by:

$$N_1 = \frac{PV}{RT} = \frac{(0.93 \text{ atm})(0.82 \text{ cm}^3)}{\left(82.06 \frac{\text{cm}^3 \text{ atm}}{K \cdot \text{mol}}\right)(289 \text{ K})} = 3.2 \cdot 10^{-3} \text{ mol}$$

Solving for D, we have:

$$D = \left(\frac{N_1}{2Ac_{10}}\right)^2 \cdot \frac{\pi}{t} = \left[\frac{3.2 \cdot 10^{-5} \ mol}{\left(36.3 \ cm^2\right)\left(2.5 \cdot 10^{-5} \frac{mol}{cm^3}\right)}\right]^2 \cdot \frac{\pi}{180 \ s} = 5.4 \cdot 10^{-6} \frac{cm^2}{s}$$

#### 4. Permeability of water across a polymer film

The rate of water loss can be found by linear regression or by simply using the first and last data points:

$$N_{i} = \frac{14.0153 g - 13.5256 g}{16 \, days} = 0.031 \frac{g}{day}$$

The molar flux is given by:

$$J_1 = \frac{N_1}{A} = \frac{0.031 \frac{g}{day} \cdot \frac{1 mol}{18.015 g} \cdot \frac{1 day}{24 \, hr} \cdot \frac{1 hr}{3600 \, s}}{85.6 \, cm^2} = 2.3 \cdot 10^{-10} \, \frac{mol}{cm^2 s}$$

From Eq. (2-2.10) we have:

$$J_1 = \frac{DH}{\ell} \Delta c_1$$

We need to find  $Ac_I$ . We first calculate the difference in the partial pressure of water across the film. From a steam table we find that at 35 °C,  $p_{sar} = 0.0555$  atm. Since the air inside the bag is saturated, we have:

$$\Delta p_s = p_{sa} - 0.75 p_{sa} = 0.25 p_{sa} = 0.25 (0.0555 atm) = 0.0139 atm$$

Assuming an ideal gas, the concentration difference is:

# <u>Diffusion In Mass Transfer Fluid Systems Solution</u> <u>Manual</u>

**Lauren Gardner** 

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